Efficient Treatment of 2,3,3,3-Tetrafluoro-2-(Heptafluoropropoxy) Propanoic Acid (GenX) by Electrochemical Degradation on a Boron-Doped Diamond Electrode

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Introduction

- manufacturing
- food packaging
- ✤ lubricants
- water-resistant coating
- fire-fighting foams





https://ntp.niehs.nih.gov/pubhealth/hat/noms/pfoa/index.html

2,3,3,3-Tetrafluoro-2-(Heptafluoropropoxy) Propanoic Acid (GenX)





- Bioaccumulation > Detected in ~ 6 millions Americans drinking water
- Long half-life in water human body
- Replace long chain with short chain



 NH_{3}

GenX Popularity



Different Methods for PFAS Removal

Treatment	PFEAs (e.g., GenX)			
Coagulation/ sedimentation/ filtration	Not effective			
Chlorination/ chloramination	Not effective			
Ozonation	Not effective			
UV/H ₂ O ₂	Not evaluated, but not expected to be effective			
PAC adsorption	Moderately effective (e.g., PFO4DA) to not effective (e.g., PFMOAA)			
GAC adsorption	Moderately effective (e.g., Nafion byproduct 2) to somewhat effective (e.g., GenX, PFO2HxA); additional data needed, bench- and pilot-testing is			
Anion exchange	ongoing Under evaluation, very effective for Nafion byproduct 2, moderately effective for GenX; removal of short-chain PFEAs such as PFMOAA needs further study			
High-pressure membranes (nanofiltration, reverse osmosis)	Not evaluated, but likely effective based on results obtained with short-chain PFASs and household reverse osmosis systems			

Compound	Material	Conditions	NaCl rejection (%)	[PFAS] ₀ (mg/L)	Time (h)	PFAS rejection (%)	References
Nanofiltration PFOA, PFBA, PFPeA, PFHxA,	NF270	200 L, 18°C, pH 6.7, 0.17–0.97 MPa,	>50%	0.001	24	93–99	Appleman et al. (2013)
PFNA, PFDA PFOS, PFBS, PFHxS	NF270	teed flow = 1 L/min 200 L, 18°C, pH 6.7, 0.17-0.97 MPa,	>50%	0.001	24	95–99	Appleman et al. (2013)
PFOS	DK	feed flow = 1 L/min 25°C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	66.4	10	96	90–99	Tang et al. (2007)
NF270 NF90	NF270	$25^{\circ}C$, pH 4, 1.38 MPa, feed flow = 1.37 L/min	56.9	10	96	90–99	Tang et al. (2007)
	25° C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	94.4	10	96	90–99	Tang et al. (2007)	
Reverse osmosis							
PFOS SG	SG	25°C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	95.2	10	96	>99	Tang <i>et al.</i> (2006, 2007)
	LFC1	25°C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	97.3	10	96	>99	Tang et al. (2007)
LFC3 BW30 ESPA3	LFC3	25°C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	98.5	10	96	>99	Tang <i>et al.</i> (2006–2007)
	BW30	25° C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	97.9	10	96	>99	Tang <i>et al.</i> (2006, 2007)
	ESPA3	25°C, pH 4, 1.38 MPa, feed flow = 1.37 L/min	94.9	10	96	>99	Tang <i>et al.</i> (2006, 2007)

(N. Merino, 2016)

Electrochemical Degradation on BDD Electrodes

Electrochemical degradation efficiency

- Electron transfer capacity
- Hydroxyl radical generation ability

- High oxygen potential
- Long life span
- With superior chemical stability
- Mechanical strength result in applying



- BDD electrodes to oxidize dyes
- Acetic acid
- Maleic acid
- Perfluorinated compounds

Electrochemical Degradation on BDD Electrodes

a) HO' with $-SO_3$ group

- HSO4
- Perfluorooctyl radical

b) HO' attack fluorine atom

• O replaces a fluorine atom > HF

C) HO' attack C-C bond

- Perfluorobutyl radical
- 1-hydroxyperfluorobutane sulfonate



FIGURE 3. Transition state for hydroxyl radical attack at (a) the $-SO_3$ site, (b) an -F site, and (c) a C-C bond. Atom key: C, gray; F, blue; S, yellow; H, white; and O, red.

(K. E. Carter, 2008)

Electrochemical Degradation on BDD Electrodes

1) Electron transfer from functional group to anode

- PFAS radical
- Perfluorooctyl radical
- 2) Decarboxylate or desulfonate of PFAS radical
- Perfluoroalkyl radical
- 3) Defluorination reaction between hydroxyl radical and Perfluoroalkyl radical



Fig. 1. Proposed pathways for electrochemical oxidation of PFCs in water.

(J. Niu, 2016)





Fig. 1. Schematic illustration of the system.

(A. Urtiaga, 2015)

(T. Ochiai, 2011)

GenX concentration:10, 100 and 1,000 ppb

Salt solution concentration:2000 mg/L sodium sulfate

Working electrode:
 10,000 ppm boron doped diamond (BDD) electrode
 (NeoCoat) cut into a 5 cm X 2.5 cm

Sampling:1-hour intervals

Chronopotentiometry was used to apply a constant current



UPLCMSMS

Shimadzu 8040 triple quadrupole mass spectrometer with an ESI source Connected to a Shimadzu Nexera UPLC C18 column, 2.1 x 50mm, with a 1.9 um particle size

Three mass analyzers in the instrument: Q1, Q2, and Q3

In Q1, isolate the intact ion of interest, so that it is the only thing that makes it through.

In Q2, fragment the ion into smaller pieces by colliding it with an inert gas; in this case, argon.

In Q3, isolate one of the resulting fragment ions, so that it is the only thing that makes it through.



The Effect of Current Density on GenX Removal

- Initial GenX concentration 10 ppb
- Different current density: 1.5, 3, and 6 mA/cm²
- Higher current density result in faster removal rate
- Almost 100% removal after 12 h for all current densities
- ✤ With 0.5 mA/cm², no removal was detected



The Effect of Initial Concentration on GenX Removal

- Current density 6 mA/cm²
- Different initial GenX concentration 10 and 100 ppb
- Almost 100% removal after 12 h for all concentrations



GenX Removal Results The Effect of Initial Concentration on GenX Removal

- Current density:
 15 mA/cm²
- Different initial GenX concentration:
 10, 100, and 1000 ppb

Sampling:30-minutes intervals

✓ For 100 ppb:
 Overall percent degradation of ~60% and ~70% respectively.

✓ For 1,000 ppb:
 Degradation of GenX slows down, resulting in
 ~13% degradation



PFOA and PFOS standard curves



Modify the electrochemical cell setup to be able to capture gas phase samples and track degradation products

Increase the efficiency

Investigate the effect of pH, boron doping, natural organic matter, etc.

